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PROCESS FOR THE PREPARATION OF ALKANEDIOL

Field of the Invention

[0001] The present invention relates to a process
for the preparation of alkanediol from alkylene
10 oxide.

Background of the Invention

[0002] Cyclic alkylene carbonates may be obtained
by contacting alkylene oxide with carbon dioxide in
15 the presence of a suitable catalyst. Such a process
has been described, for example, in EP-A-119840. In
addition, the cyclic alkylene carbonate may be
further reacted. A conventional further process
comprises hydrolysis of the cyclic alkylene carbonate
20 to produce a diol as is described in US Patent No.
5,847,189.

[0003] U.S. Patent No. 6,407,279 discloses the
integration of the above steps such that cyclic
carbonate may be fed to the transesterification
25 reaction zone without purification of the cyclic
carbonate. U.S. Patent No. 6,407,279 also describes
that the elimination of the cyclic carbonate
purification step causes elimination of two vacuum
distillation columns and gives a yield benefit by
30 eliminating losses of cyclic carbonate attributable
to the purification steps. The carbonation reaction
of U.S. Patent No. 6,407,279 is carried out at a
pressure in the range from about 500 psia to about
1000 psia while the transesterification reaction is
35 carried out at a pressure of about 100 psia to 300
psia.

Summary of the Invention

[0004] The present invention is directed to a process for the preparation of alkanediol, which process comprises:

- 5 (a) contacting alkylene oxide with carbon dioxide in the presence of catalyst to obtain a first liquid reaction mixture containing cyclic carbonate,
 - (b) optionally removing carbon dioxide and/or alkylene oxide,
 - 10 (c) increasing the pressure of the liquid reaction mixture obtained in step (a) and/or (b),
 - (d) contacting the pressurized first reaction mixture obtained in step (c) with water in the presence of catalyst to obtain a second reaction mixture
 - 15 containing alkanediol and carbon dioxide,
 - (e) separating the second reaction mixture into a liquid effluent and a gaseous effluent containing carbon dioxide, and
 - (f) recycling at least part of the gaseous effluent
 - 20 containing carbon dioxide to step (a),
- in which process the pressure in step (d) is higher than the pressure in step (a).

Detailed Description of the Invention

25 **[0005]** We have now found that an integrated process may be improved further. The improvement eliminates the need to increase the pressure of a gas or a mixture of gas and liquid.

[0006] Increasing the pressure of fluids may be
30 done in many ways. The means employed usually is centrifugal force or transfer of momentum. In the chemical industry, centrifugal pumps or compressors are typically used, which are based on the principle of producing kinetic energy by the action of

centrifugal force and then converting this energy into pressure by efficiently reducing the velocity of the flowing fluid. If transfer of momentum is used, one fluid is decelerated in order to transfer its momentum to a second fluid. Jets and eductors make use of transfer of momentum.

[0007] A common phenomenon in increasing the pressure of fluids is that increasing the pressure of a gas or a mixture of gas and liquid is more difficult than increasing the pressure of a liquid only. Apparatus for increasing the pressure of a gas or a mixture of gas and liquid have the disadvantage that they more easily fail in operation and are expensive.

[0008] The present invention makes it possible to operate while increasing the pressure of a liquid instead of having to increase the pressure of a gas or a mixture of gas and liquid.

[0009] In process step (a) of the present invention, the alkylene oxide is contacted with carbon dioxide in the presence of catalyst. Several catalysts are known to be suitable for such a process. Preferably, the catalyst is a homogeneous phosphorus containing catalyst. Phosphorus containing compounds which are suitable catalysts are phosphine compounds and phosphonium compounds. The catalyst preferably is a homogeneous phosphonium catalyst, more specifically a phosphonium halide catalyst. It was found especially advantageous to employ a tetraalkylphosphonium halide catalyst, more specifically a tributyl-methyl phosphonium iodide.

[0010] The catalyst may be either added as such or may be formed in-situ. The reaction mixture which is added to step (a), preferably is substantially

free of water. The amount of water is preferably less than 5 %wt, more preferably less than 1 %wt, most preferably less than 0.1 %wt, based on total amount of reaction mixture added.

5 **[0011]** The alkylene oxide for use in the present invention preferably is propylene oxide. The use of propylene oxide starting compound in the present invention, makes that propylene carbonate is formed in step (a) which leads to the manufacture of
10 1,2-propanediol or monopropylene glycol in step (b). In such process, the alkanediol is 1,2-propanediol and the alkylene oxide is propylene oxide.

[0012] The carbon dioxide may be either pure carbon dioxide or carbon dioxide containing further
15 compounds. Carbon dioxide which is especially suitable for use in the present invention is carbon dioxide which has been separated off in subsequent steps of the present process. Carbon dioxide may either be separated off directly after the alkylene
20 oxide has reacted with carbon dioxide or at a later stage.

[0013] Carbon dioxide is produced in the reaction of the cyclic alkylene carbonate with water. Therefore, it is especially attractive to separate
25 carbon dioxide and recycle the carbon dioxide thus obtained to step (a) either as such or after having been purified. The extent to which the carbon dioxide is purified depends on the nature and the amounts of contaminants present in the carbon dioxide. These
30 again depend on the exact reaction conditions and purification steps of the process.

[0014] Operating conditions for step (a) are known in the art. Preferred operating conditions will generally comprise a temperature of from 50 °C to

200 °C, more specifically 100 °C to 150 °C, and a pressure of at least 2×10^5 N/m², more specifically a pressure of from 2 to 100×10^5 N/m², most specifically of from 3 to 40×10^5 N/m². Preferably, process step (a) is carried out at a pressure of from 10 to 30×10^5 N/m².

[0015] The catalyst may be added to the reactor in any form known to be suitable to someone skilled in the art. Generally, the catalyst will be added as such or as a solution of the catalyst preferably in an inert solvent such as a cyclic carbonate or alkylene glycol. The catalyst may be added either to the alkylene oxide or to the carbon dioxide or to the mixture of both. Preferably, the catalyst solution is added to the reactor containing the mixture of alkylene oxide and carbon dioxide.

[0016] The reaction mixture obtained in step (a) is preferably used without further purification in the manufacture of alkanediol. However, some purification of the reaction mixture may be carried out. It may be advantageous to remove carbon dioxide and/or alkylene oxide from the first reaction mixture. The carbon dioxide and/or unconverted alkylene oxide which are separated off may be recycled to step (a). Separation of carbon dioxide and/or unconverted alkylene oxide may substantially reduce the volume of the reaction mixture to be subjected to steps (c) and (d). Additionally, the removal of carbon dioxide and/or unconverted alkylene oxide reduces the risk of cavitation in a pump.

[0017] In step (c), the pressure of the first reaction mixture obtained in step (a) and/or (b) is increased. The increase in pressure may be done in

any way known to someone skilled in the art.
Generally, a pump will be used which is known to be
suitable for this specific application such as a
centrifugal pump.

- 5 **[0018]** The pressurized liquid obtained in step
 (c) will generally have a pressure of from 1 to
 100 x 10⁵ N/m², more specifically of from 3 to
 60 x 10⁵ N/m², more specifically of from 5 to
 50 x 10⁵ N/m².
- 10 **[0019]** In a preferred embodiment, the feed
 subjected to step (d) contains a substantial amount
 of alkylene oxide. The presence of alkylene oxide may
 be due to the fact that part of the alkylene oxide
 has not been converted in step (a) and/or to the fact
15 that alkylene oxide is added either before or during
 step (d). Preferably, the amount of alkylene oxide
 and cyclic carbonate in step (d) is such that the
 molar ratio of alkylene oxide to cyclic carbonate is
 from 0.01:1 to 1:1, more preferably from 0.02:1 to
20 0.6:1, more preferably from 0.03:1 to 0.4:1, more
 preferably from 0.04:1 to 0.3:1, more preferably from
 0.05:1 to 0.2:1. Most preferably, the molar ratio of
 alkylene oxide to cyclic carbonate is from 0.08:1 to
 0.15:1.
- 25 **[0020]** In the process according to the present
 invention, it is preferred that process step (a) is
 carried out with a homogeneous catalyst and step (d)
 is carried out with a heterogeneous catalyst. More
 preferably, the homogeneous catalyst present in
30 step (a) is not removed until after step (d). This
 has the advantage that the homogeneous catalyst of
 step (a) may be active in the conversion of the
 alkylene oxide if alkylene oxide is still present in
 step (d). Removal of a limited amount of the

homogeneous catalyst such as in distillation of part or all of the reaction mixture, will generally still leave sufficient homogeneous catalyst in the reaction mixture to serve its purpose in step (d) of the present process.

[0021] In step (d), at least part of the pressurized reaction mixture obtained in step (c) is hydrolyzed. Although it is possible to process only part of the product of step (c), generally, substantially all of the pressurized liquid obtained will be subjected to step (d).

[0022] In the present process, water is added in step (d) to the pressurized reaction mixture obtained in step (c). Although alcohol such as methanol may be added in addition to water, it is preferred to add water only. The presence of water only results in a more limited number of products, which is advantageous in the subsequent separation of products.

[0023] The catalysts for use in the present invention are known in the art. Preferably, the catalysts are heterogeneous catalysts. Examples of such catalysts comprise solid inorganic compounds such as alumina, silica-alumina, alumina carrying a copper compound, silica-alumina carrying a copper compound, silica-magnesia, aluminosilicate, gallium silicate, zeolites, metal-exchanged zeolites, ammonium-exchanged zeolites, zinc on a support, lanthanum on a support, a mixture of aluminium and magnesium (hydr)oxide and ion-exchange resins.

[0024] Preferably, the catalyst employed in step (d) is chosen from the group consisting of a mixture of aluminium and magnesium (hydr)oxide, zinc on a support, lanthanum on a support and alumina. These

catalysts will be described hereinafter in more detail.

5 **[0025]** The mixture of aluminium and magnesium (hydr)oxide preferably has a magnesium to aluminium molar ratio in the range of from 3 to 50, more preferably of from 4 to 20. In the preparation of the catalyst, generally a so-called mixed magnesium/aluminium hydroxide is formed. However, under working conditions, mixed magnesium/aluminium
10 oxides may be present. Our reference to a mixture of aluminium and magnesium (hydr)oxide covers both mixtures of aluminium and magnesium hydroxide and mixtures of aluminium and magnesium oxide and a combination of both mixtures. These mixtures were
15 found to give the highest activity at a molar ratio of more than 3, preferably more than 4. A preferred range was found to be from 4 to 20, more specifically from 5 to 15, most specifically from 5 to 10. Preferred catalysts are described in International
20 application No. PCT/EP02/12640.

[0026] In another preferred embodiment of the present invention, the catalyst comprises a lanthanum compound on a support. A preferred catalyst comprises at least 7 %wt of lanthanum supported on a support.
25 The lanthanum compound preferably is La_2O_3 or a precursor thereof. Under reaction conditions, this lanthanum compound may be temporarily and/or reversibly converted due to the reaction conditions into lanthanum hydroxide ($\text{La}(\text{OH})_3$), lanthanum-oxyhydroxide ($\text{LaO}(\text{OH})$) and/or corresponding
30 alcoholate species such as ($\text{La}(\text{OR})_3$ or $\text{LaO}(\text{OR})$).

[0027] As a support for the lanthanum containing catalyst any suitable support may be used. The support preferably is substantially inert under the

reaction conditions and is provided with sufficient mechanical strength. Potential supports comprise clay minerals, inorganic supports such as Al_2O_3 , SiO_2 , MgO , TiO_2 , ZrO_2 , ZnO and mixtures thereof. Other
5 examples are a kaolinite, a hallosyte, a chrysotile, a montmorillonite, a beidellite, a hectorite, a sauconite, a muscovite, a phlogopite, a biotite, a hydrotalcite and talc. Particularly preferred are the inorganic supports selected from the group consisting
10 of Al_2O_3 , SiO_2 , MgO , TiO_2 , ZrO_2 , ZnO and mixtures thereof.

[0028] The lanthanum containing catalyst preferably comprises at least 7 %wt of lanthanum, more specifically in the range of from 7 to 40 %wt of
15 lanthanum based on total amount of catalyst. The lanthanum containing catalyst may be produced using any suitable method. A preferred method comprises impregnating a support with a lanthanum containing salt, and subsequently drying and calcining the
20 impregnated support. After impregnation, the impregnated support may be dried and subsequently calcined. Calcination is generally carried out at a calcination temperature from between 120 °C to 700 °C. The catalyst activity may be increased even
25 further if the catalyst is calcined at a temperature in the range of from 350 °C to 600 °C. Preferred catalysts are described in PCT patent application PCT/EP02/12638.

[0029] A further catalyst which is especially
30 suitable for use in step (d) of the present invention is a zinc supported catalyst. The support preferably is selected from the group consisting of Al_2O_3 , SiO_2 , MgO , TiO_2 , ZrO_2 , Cr_2O_3 , carbon and mixtures thereof.

The zinc supported catalyst may be prepared by impregnation of silica, alumina or mixtures of aluminium and magnesium (hydr)oxide with a zinc nitrate solution. Preferably, the zinc supported catalysts comprise at least 15 %wt of zinc on a support having a surface area of at least 20 m²/g, more preferably at least 40 m²/g. Preferred catalysts are described in the patent applications claiming priority of European patent application No. 02256347.2.

[0030] A further catalyst which is preferably used is a catalyst consisting of alumina. Preferably, the alumina is gamma-alumina.

[0031] Step (d) of the present process is preferably carried out at a temperature of from 50 °C to 300 °C, preferably of from 80 °C to 250 °C, more specifically of from 100 °C to 200 °C. The pressure may vary widely, and preferably is at least 1 x 10⁵ N/m², more specifically at least 2 x 10⁵ N/m².

The pressure generally will be at most 100 x 10⁵ N/m², more specifically at most 70 x 10⁵ N/m², most specifically at most 60 x 10⁵ N/m². Preferably, the pressure in step (d) is of from 5 to 50 x 10⁵ N/m², more specifically of from 15 to 35 x 10⁵ N/m².

[0032] The pressure at which step (d) is operated is higher than the pressure at which step (a) is operated. Generally, the pressure in step (d) will be at least sufficient to compensate for any pressure drop in the process as a whole. Preferably, the pressure in step (d) will be at least 0.1 x 10⁵ N/m² higher than the pressure in step (a), more specifically at least 1 x 10⁵ N/m² higher, preferably

at least 2×10^5 N/m² higher. The pressure in step (d) generally will be at most 50×10^5 N/m² higher than the pressure in step (a), more specifically at most 20×10^5 N/m², more specifically at most 15×10^5 N/m², most specifically at most 10×10^5 N/m².

[0033] In step (e), the second reaction mixture is separated into a liquid effluent and a gaseous effluent containing carbon dioxide. Such separation may be carried out by sending the second reaction mixture to an empty vessel. The reaction mixture separates into a carbon dioxide rich gaseous phase and a liquid phase. The gaseous effluent containing carbon dioxide obtained in step (e) preferably is recycled directly to step (a), optionally after having been combined with fresh carbon dioxide. A direct recycle is considered to be a recycle in which no further compounds are separated off. However, the gas which is recycled directly may have been subjected to treatments causing a change in temperature and/or pressure such as heat exchange with one or more other streams either of the present process or of a different process.

[0034] The liquid effluent obtained in step (e) may be separated further. Preferably, the separation comprises (g) separating the liquid effluent obtained in step (e) further into a gaseous effluent rich in carbon dioxide and a liquid effluent, (h) contacting with water the gaseous effluent rich in carbon dioxide obtained in step (g), and (i) sending the water used in step (h) to step (d). The separation of step (g) preferably is carried out at a pressure of from 0.1 to 20×10^5 N/m², more specifically of from

1 to 15×10^5 N/m², most specifically of from 1 to 2×10^5 N/m². Alkanediol may be separated from the liquid effluent obtained in step (g).

5 **[0035]** In step (f), at least part of the gaseous effluent containing carbon dioxide is recycled to step (a). The carbon dioxide may be recycled to step (a) without the need to increase its pressure. Advantageously, the process according to the present invention may be carried out without increasing the
10 pressure of any of the streams present in step (a) to (f) besides the increase in pressure attained in step (c).

[0036] Preferably, alkanediol is separated from the second reaction mixture. The alkanediol may be
15 separated from the reaction mixture obtained in step (d), (e) and/or (g) in any way known in the art. A preferred separation comprises distillation of the second reaction mixture, preferably by vacuum distillation, optionally followed by further
20 distillation of one or more of the distillate fractions and/or bottom fractions. One or more of the fractions separated will have a high content of alkylene glycol. Alkylene glycol obtained by distillation will usually be sufficiently pure to use
25 as such. If required, small amounts of by-products may be removed separately.